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WOOD CHAR-WATER SORPTION COEFFICIENTS OF ORGANIC SORBATES

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Polyparameter Linear Free Energy Relationship for Wood Char-Water Sorption Coefficients of Organic Sorbates

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Abstract

Black carbons (BCs), including soots, chars, activated carbons, and engineered nanocarbons, have different surface properties, but we do not know to what extent these affect their sorbent properties. To evaluate this for an environmentally ubiquitous form of BC, biomass char, we probed the surface of a well-studied wood char using 14 sorbates exhibiting diverse functional groups and then fit the data with a polyparameter linear free energy relationship (ppLFER) to assess the importance of the various possible sorbate-char surface interactions. Sorption from water to water-wet char evolved with the sorbate's degree of surface saturation and depended on only a few sorbate parameters:

$$\log K_d(\text{L/kg}) =$$

$$[(4.03 \pm 0.14) + (-0.15 \pm 0.04) \log a_i] V + [(-0.28 \pm 0.04) \log a_i] S + (-5.20 \pm 0.21) B$$

where a_i is the aqueous saturation of the sorbate i , V is McGowan's characteristic volume, S reflects polarity, and B represents the electron-donation basicity. As generally observed for activated carbon, the sorbate's size encouraged sorption from water to the char, while its electron donation/proton acceptance discouraged sorption from water. However, the magnitude and saturation dependence differed significantly from what has been seen for activated carbons, presumably reflecting the unique surface chemistries of these two BC materials and suggesting BC-specific sorption coefficients will yield more accurate assessments of contaminant mobility and bioavailability and evaluation of a site's response to remediation.

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Keywords

Sorption, Wood char, Hydrophobic organic compounds (HOCs), Polyparameter linear free energy relationship (ppLFER), Black carbon (BC)

1 INTRODUCTION

2

3 In an effort to manage contaminated sediments and soils, regulators try to use data
4 on solid phase concentrations of organic contaminants to identify deposits that pose
5 unacceptable toxic risks. Commonly, this is done by assuming equilibrium partitioning
6 of the compounds among the solid phases, porewater or soil gas, and associated
7 organisms [1]. The key parameter allowing us to use sediment/soil concentrations in this
8 model is the solid-water sorption coefficient, K_d [(mol/kg_{solid})/(mol/L_{water})]. In the case of
9 contaminated sediments, this allows us to estimate porewater concentrations, C_w , from
10 the ratio, C_{sed}/K_d .

11 Until now, regulators have assumed that K_d for most nonionic contaminants is
12 given by the product, $f_{oc}K_{oc}$, where f_{oc} is the organic carbon content of the sediment
13 (kg_{oc}/kg_{solid}) and K_{oc} is the organic carbon-normalized solid-water partition coefficient
14 [(mol/kg_{oc})/(mol/L_{water})]. However, such sorption modeling has been found to be
15 extremely inaccurate at many sites [2,3]. If it were accurate, then one should find close
16 correspondence between porewater concentrations and sediment concentrations
17 normalized by $f_{oc}K_{oc}$. Instead, measured values of C_w are commonly up to a *factor of 100*
18 less than $C_{sed}/f_{oc}K_{oc}$ [4]! Likewise, biota-sediment accumulation factors (BSAFs)
19 measured for a wide range of benthic infauna are often 1 to 2 orders of magnitude below
20 the corresponding equilibrium partitioning expectation [5-7]. This situation suggests that
21 there is a major problem with respect to estimating solid-water partition coefficients
22 using only an $f_{oc}K_{oc}$ model.

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23 We now know that sediments and soils include "black carbons" (BCs) such as
24 soots, biomass chars, and coal dust residues, and that these special components of the
25 total organic carbon must be distinguished from the rest of the organic matter to estimate
26 accurately K_d values of many contaminants [8-14]. Thus, sorption estimations can be
27 greatly improved by using an extended expression that includes black carbon as a
28 separate sorbent [10]

29

$$30 \quad K_d = f_{oc}K_{oc} + f_{BC}K_{BC}C_w^{(n-1)} \quad (1)$$

31

32 where f_{oc} is now the non-BC organic carbon weight fraction in the sediment, f_{BC} is the
33 BC weight fraction, K_{BC} is the compound specific BC-water adsorption coefficient, and
34 $C_w^{(n-1)}$ is the dissolved sorbate concentration of compound raised to a power, $n-1$, to
35 reflect the nonlinearity of adsorption to the BC surface. To date, the majority of available
36 K_{BC} values are derived from studies using engineered, granular activated carbon (GAC)
37 as a sorbent, but distinct BCs may have different sorption coefficients from GAC. If so,
38 then solid-water partitioning models would be improved by the use of the appropriate K_{BC}
39 when the sorbent identity is known (e.g., near a coal storage site or after application of an
40 engineered biochar). In the present study, we explore the sorption parameters for a
41 biochar (K_{char} and n_{char}) for a structurally diverse array of sorbates and compare those to
42 sorption parameters for GAC in order to determine if BC-specific sorption parameters are
43 needed.

44 Chars, themselves, are ubiquitous and structurally diverse [15] and can have a
45 wide range of surface areas and surface functionalities, depending on the conditions of

46 their formation [16, 17]. However, chars formed at greater than about 400°C typically
47 have predominantly aromatic surface character [17-19] and some oxygen-containing
48 functionalities [20, 21]. Further, biochars are increasingly investigated as “green”
49 sorbates, as they can be made from waste biomaterials, and they have abundant natural,
50 incidental, and engineered sources globally (Figure 1).

51 Hence, here we characterize sorption of 14 diverse sorbates to a wood char
52 formed at 450°C . After determining the isotherms, polyparameter linear free energy
53 relationship (ppLFER) modeling was used to identify the most important intermolecular
54 interactions controlling sorption to this water-wet char. The choice of model sorbates
55 was intended to capture the widest degree of variability in the Abraham/McGowan [25,
56 26] sorbate parameter space with a relatively small number of sorbates that are liquids at
57 room temperature. Overall, our goals were to (a) enable prediction of partitioning
58 coefficients for untested compounds whose parameters fall within our tested range for
59 this particular wood char and (b) add to the understanding of the fundamental
60 mechanisms of sorption from water to unique biochars. We note that applying the
61 resultant ppLFER outside the training set parameter space (e.g., extrapolating to estimate
62 K_{BC} values for PCBs) may result in large errors in estimated K_{ds} , especially as steric
63 issues related to the sorbates' surface interactions and pore access can arise.

64

65

EXPERIMENTAL METHODS

66

67 *Chemical sorbates.*

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68 We used 14 sorbates (Table 1) with varied functional groups, covering a range of
69 the ppLFER parameter space (i.e., V from 0.715 to 1.154, E from 0 to 0.871, S from 0 to
70 1.11, A from 0 to 0.37, and B from 0 to 0.51). While these probe compounds do not
71 cover the entire known range of the parameters [25, 26], they do represent diverse
72 intermolecular forces and have a relatively broad range in aqueous solubilities (Table 1).
73 Any ppLFER can only be justifiably applied within the tested Abraham/McGowan
74 parameter space, rather than outside of it (i.e., the V , E , S , A , and B of a compound must
75 fall within the range tested here if the ppLFER is to give accurate results). Sorbate-
76 saturated aqueous solutions were prepared by equilibrating excess quantities of each
77 sorbate with 18M Ω UV-oxidized water for at least 1 wk in pre-combusted, ground-glass-
78 stoppered flasks.

79

80 *Char sorbent.*

81 Wood char, prepared from chestnut hardwood pyrolyzed at 450°C as described in
82 Hammes et al. [21; see also 27, 28], was purchased from the Schmidt Laboratory at the
83 University of Zurich (Supplemental Data, Table S1). To ensure uniform sorbate
84 exposure to char surfaces and ultimately aid in gravitational settling of the char, the fine
85 char particles were dispersed in ethyl acetate, spread over pre-combusted, acid-washed,
86 Ottawa sand, and then stirred semi-continuously while air drying. The char-quartz
87 mixture was further dried at 60°C for 72 h, with stirring every 12 h. The weight percent
88 carbon contents of the quartz, char, and the char-quartz mixture were 0.016 ± 0.006 , 71.7
89 ± 0.2 , and 1.1 ± 0.2 % C, respectively, as determined using a CHN analyzer (Vario EL,
90 Elementar America, Inc.) operated at a combustion temperature of 950 °C. Specific areas

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91 for quartz, char, and the char-quartz mixture were 3.3, 5.9, and 3.6 m² g⁻¹, respectively, as
92 determined by single-point nitrogen BET (Brunauer-Emmett-Teller) testing (PMI
93 Analytical Testing, Ithaca, NY). Note that Hammes et al. [21] reported 2.0 m² g⁻¹ for this
94 particular wood char.

95

96 *Sorption equilibration experiments.*

97 All batch sorption experiments were conducted in pre-combusted, 7-mL, 18-mL,
98 or 50-mL ground-glass-stoppered centrifuge tubes. All-glass containers were used to
99 avoid sorbate losses to Teflon™ or other polymers [29-31]. Sorbent (i.e., char-quartz
100 mixture) and sorbent-free (i.e., quartz only) samples were pre-wet with 18 MΩ water for
101 at least 1 wk prior to sorbate addition. Serial dilutions of the water-saturated sorbate
102 stocks were gravimetrically prepared (at 0.1, 0.01, 0.001, and 0.0001 aqueous saturation)
103 and then immediately added to triplicate sorbent containers. Headspace was minimized
104 to avoid sorbate loss to the vapor phase. Sorbate concentrations were quantified
105 following 7-to-14 d equilibration times, which we determined was sufficient to establish
106 equilibrium (based on a toluene sorption time-series (Supplemental Data, **Figure S1**;
107 **Table S2**). To minimize the influence of suspended colloids on the measured dissolved
108 aqueous concentrations of sorbate, each test tube was centrifuged at 1150 g for at least 90
109 min prior to sorbate quantification. Recall that the char itself was spread over quartz sand
110 (through the use of an ethyl acetate carrier) to ensure uniform exposure of the char and to
111 aid gravitational settling.

112 As sorption to char is a surface process, we chose to probe the char surface as a
113 function of sorbate *activities*, rather than *concentrations*. Here, recognizing that these

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114 liquid sorbate's solubilities represent 100% saturation in solution, the fractional saturation
115 in solution also corresponds to the same degree of saturation (or chemical activity) on the
116 char surface at solution-surface equilibrium in a batch experiment. This allowed us to
117 investigate the effect of increasing surface coverage between highly variable sorbates.
118 Since the probe sorbates' have a broad range of aqueous solubilities, and comparison at
119 equal concentrations would either unnecessarily limit the range of chemical loadings (i.e.,
120 for the most water-soluble species) or result in the formation of a pure sorbate phase (i.e.,
121 for the least soluble species), which would confound the results.

122

123 *Sorbate quantification and sorption calculation.*

124 Analytes with relatively low aqueous solubilities (<6,000 mg/L) were quantified
125 using a purge and trap pre-concentrator (Tekmar LCS 2000) interfaced to a gas
126 chromatograph (GC; Perkin Elmer AutoSystem XL) with a flame ionization detector
127 (FID) for hydrocarbons or an electron capture detector (ECD) for halogenated
128 compounds. Analytes with relatively high aqueous solubilities (>6,000 mg/L) were
129 quantified via direct aqueous injection onto a GC-FID (Carlo Erba HRGC 5300 Mega
130 Series MFG 500). Both instruments were equipped with a DB-624 capillary column (60
131 m x 3.80 μ m x 0.320 mm) and temperature programs varied with the analyte.

132 The average aqueous sorbate concentration in char-free control tubes (i.e., quartz
133 only; n=3) was compared to the aqueous sorbate concentration in char-containing tubes
134 (i.e., C_w), where the difference was attributed to sorption to char. This mass difference
135 was normalized to the mass of char sorbent to give the concentration of sorbate on the
136 solid char (i.e., C_s). For hexane and heptane, which have relatively high air-water

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137 partition coefficients, we also accounted for the mass of sorbate in test tube bubbles that
138 evolved during the course of the equilibration (<1 mL, where the volume was deduced by
139 changes in weight).

140

141 *Sorption isotherms.*

142 The experimentally-determined C_s and C_w data were fit to the log-transformed
143 Freundlich equation

144

$$145 \log C_s = \log K_f + n \log C_w \quad (2)$$

146

147 where C_s and C_w are equilibrium concentrations in the solid phase (mg/kg) and aqueous
148 phase (mg/L), respectively, and K_f [(mg/kg)/(mg/L)^{*n*}] and n (dimensionless) are the
149 Freundlich coefficient and Freundlich exponent, respectively.

150

151 *Polyparameter linear free energy relationship.*

152 All measures of K_d (i.e., each C_w/C_s pair) were used to evaluate the dependence
153 of K_d on sorbate properties (i.e., the Abraham/McGowan parameters) by fitting the
154 saturation-dependent ppLFER (Eqn. 3).

$$155 \log K_{d,activity}(\text{L/kg}) = (v_1 + v_2 \log a_i)V + (e_1 + e_2 \log a_i)E + (s_1 + s_2 \log a_i)S \\ 156 + (a_1 + a_2 \log a_i)A + (b_1 + b_2 \log a_i)B + c_1 + c_2 \log a_i \quad (3)$$

157 where V (in cm³ mol⁻¹/100) is the sorbate's McGowan characteristic volume, E (in
158 cm³/10) is the excess molar refraction, S is the polarity/polarizability parameter, A and B
159 are the hydrogen acidity and basicity, respectively, and $a_i = C_{iw}/C_{iw,sat}$, is the ratio of the

160 sorbate i 's concentration to its (liquid) solubility. Coefficients were determined both by
161 backward and forward stepwise multiple linear regression analysis of experimental values
162 using Microsoft™ Excel and StatPlus™. In the case of backward fitting, the significance
163 of each term in equation 3 was evaluated using a t test to determine the probability that
164 the coefficient was different from zero. Insignificant terms were systematically
165 eliminated one at a time and then the regression analysis was repeated until only
166 significant correlation coefficients remained (i.e., via backward stepwise multiple
167 regression analysis) and the ANOVA factor, F , was maximized. Given a data set of 128
168 observations, 6-12 parameters could be fit meaningfully, but we ultimately found only 4
169 parameters proved to be significantly different from zero in the optimized ppLFER fit.
170 For comparison, a forward stepwise multiple linear regression analysis yielded the same
171 significant terms and coefficients (Supplemental Data, [Table S3](#)).

172

173

RESULTS

174

175 *Sorption kinetics.*

176 Sorption time courses were assessed using toluene, which has a similar aqueous
177 diffusivity ($ca. 10^{-5} \text{ cm}^2 \text{ s}^{-1}$) as our other probe sorbates. Dissolved toluene
178 concentrations approached equilibrium in less than 1 week (Supplemental Data, [Figure](#)
179 [S1](#)), and thus, we concluded that our incubation timeframe should be at least 1 wk to
180 establish equilibrium, while at the same time not suffering losses during the incubations
181 (e.g., since bubbles appeared). More sorptive probe compounds, such as pyrene or
182 polychlorinated biphenyls, experience even greater retardation of diffusive transport into

183 porous char. Thus, they require longer equilibration times and are not yet included in this
184 set of probe compounds.

185

186 *Sorption isotherms.*

187 The Freundlich equation (Eqn. 1) fit the data for each sorbate well, with
188 correlation coefficients of at least 0.96, except for heptane ($R^2 = 0.77$) and diisopropyl
189 ether ($R^2 = 0.87$; Figure 2 and Table 2). Each isotherm was constructed using at least
190 eight data points, except for 1-heptanol ($N=6$). Within each compound class (e.g.,
191 alkanes, ethers, and alcohols), sorbates with the highest aqueous solubility exhibited the
192 lowest affinity for char (lowest sorption), except for diethylether (Figure 2). For alkanes,
193 alcohols, and ketones, the seven-carbon sorbate always had a larger K_f than the respective
194 six-carbon compounds (Table 2), likely reflecting their increased van der Waals
195 interactions with the char surface and increased cost of cavity formation in water due to
196 the addition of methylene groups. Although diethyl ether was the most soluble ether,
197 implying greater relative affinity for the solution phase, its larger K_f value compared to
198 MTBE and diisopropyl ether suggested intermolecular interactions with the char that
199 were not applicable to the branched ethers, such as due to steric effects.

200

201 *Polyparameter linear free energy relationships.*

202 To capture the saturation-dependent behavior of sorption, we fit the expanded
203 LFER expression (Eqn. 3), which includes a dependence on aqueous saturation ($a =$
204 $C_w/C_{w,sat}$), noting that aqueous saturation and sorption saturation must occur together in
205 our experiment if we successfully achieved equilibration. Using the 128 independent

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206 $K_{d,activity}$ observations (Figure 3), we optimized the fit via the multiple regression statistic

207 F and found

208

209 $\log K_{d,activity}(\text{L/kg}) = [(4.03 \pm 0.14) + (-0.15 \pm 0.04) \log a]V$

210

211 $+ [(-0.28 \pm 0.04) \log a]S + (-5.20 \pm 0.21)B,$

212

213 $R^2 = 0.98, N=128, SE=0.41$ (4)

214

215 For our data set, the coefficients for the *A* (hydrogen acidity/electron accepting capacity)

216 and *E* (molar refraction/polarizability) terms were not significantly different from zero,

217 suggesting these parameters did not substantially influence char-water sorption. Note

218 that the tested range of *A* was comparatively small (0 to 0.37), and dependence on *A* may

219 emerge if the data set were expanded. Further, the ppLFER should only be employed for

220 sorbates whose Abraham/McGowan parameters fall within the tested parameter space

221 (Table 1). Char-water partitioning depended directly on the dispersion interactions (*V*

222 term), inversely on the electron donating character (*B* term), and weakly on the sorbate's

223 polarizability (*S* term). Interestingly, the *V* term exhibited some dependence on

224 saturation, becoming more important at higher dilution; the *B* term did not exhibit

225 significant dependence on saturation over the investigated range, and the *S* term was only

226 important at low activities (e.g., $a < 0.001$). The physical-chemical implications of these

227 dependencies are discussed below.

228

229

DISCUSSION

230

231 *Consistency of ppLFER with previous observations.*

232 Due to the prevalent use of activated carbon in water remediation applications,
233 several research groups have previously developed activated carbon-water partitioning
234 LFERs for organic compounds. While the exact coefficients differ (Table 3) [32-36],
235 likely due to differences in GAC character and perhaps some experimental problems
236 associated with assuming equilibrium before it is reached (Supplemental Data, Table S2),
237 the important sorbate parameters are consistent: the molar volume (V) and electron-
238 donation basicity (B) always exhibit the largest influence on the distribution coefficient,
239 K_d . The dispersion term (V) always encourages sorption and the electron-donating
240 basicity (B) of a sorbate always reduced sorption, and both were clearly different from
241 zero.

242 The positive coefficient on the V term (Eqn. 4) largely results from the favorable
243 free energy change associated from moving out of water to a hydrophobic surface. The
244 activity dependency suggests more complete sorbate removal at low saturations
245 (increasing influence of V term at low surface coverage), consistent with the view that the
246 most favorable sorption sites involve deeper sorbate penetration into the porous char.

247 The negative impact of the B term implies that loss of hydrogen-bond donating
248 interactions between the sorbate and solvent water are not replaced by interactions with
249 the water-wet char. This is consistent with the expectation that aromatic pi electrons in
250 the char can donate electron density to a hydrogen-bonding sorbate but cannot accept
251 electron density from electron-donating sorbates [37]. The absence of aqueous saturation

252 dependence of the B term for char sorption suggests that this effect is independent of the
 253 surface coverage on the char. In other words, the saturation independent character and
 254 negative coefficient of B may simply reflect a constant “penalty” of sorbate removal from
 255 water, irrespective of sorbate position within the char.

256 Other terms made smaller contributions to K_d , as was observed for activated
 257 carbon (see Table 3). In the case of the wood char, the contribution of the polarizability
 258 parameter (S) to K_d was weak but activity dependent, becoming more positive at lower
 259 sorbate coverage. This may imply that dipole-induced dipole or dipole-dipole
 260 interactions with char are stronger at lower char surface coverages. At higher degrees of
 261 saturation, the dipole-induced dipole and dipole-dipole interactions with water and water-
 262 wet char may be roughly equivalent, and thus, the effect of the S term decreases in
 263 significance.

264

265 *Interpretation of Freundlich parameters.*

266 The Freundlich isotherm parameters K_f and n are influenced by a sorbate’s
 267 structural parameters, and the ppLFER’s dependence on chemical aqueous saturation
 268 allowed us to investigate this relationship. The distribution coefficient, K_d , is equal to
 269 C_s/C_w , and chemical activity, a , expresses the saturation level, $C_w/C_{w,sat}$; substituting
 270 these ratios into Equation 4 and rearranging yields

271

272 $\log C_s = (4.03V - 5.20B) + (0.15V + 0.28S) \log C_{w,sat} +$

273

274 $(-0.15V - 0.28S + 1) \log C_w$ (5)

275

276 This equation (Eqn. 5) has the form of the log-transformed Freundlich isotherm
 277 expression (Eqn. 1), $\log C_s = \log K_f + n \log C_w$, and can thus be solved to determine log
 278 K_f and n in terms of the sorbate parameters, V , S , and B .

279

$$280 \log K_f [(mg/kg)/(mg/L)^n] = (4.03V - 5.20B) + (0.15V + 0.28S) \log C_{w,sat} \quad (6)$$

281

282 and

283

$$284 n = -0.15V - 0.28S + 1 \quad (7)$$

285

286 The accuracy of this approach is suggested by the goodness of fit of the observed data
 287 with those predicted by Equations 6 and 7 (Figure 4). As was observed for granular
 288 activated carbon (GAC) [32], the V and B terms are also the major contributors to the
 289 Freundlich coefficient observed for char. Dispersive forces (captured by the V term)
 290 encourage sorption and increase K_f , whereas electron donation capacity (reflected by the
 291 B term) decreases K_f . A sorbate's polarizability (S term) makes a minor contribution to
 292 the Freundlich coefficient and that contribution is higher for solutes with larger aqueous
 293 solubilities. For example, a typical hydrogen-bond accepting sorbate could have $V \approx 1$,
 294 $B \approx 0.5$, $S \approx 0.5$, and $\log C_{w,sat} \approx \log(1 \text{ mg/L}) = 1$, and thus, $\log K_f \approx 4.18 - 0.26 + 0.14 \approx 4$,
 295 where the terms correspond to the contributions of V , B , and S , respectively. In contrast,
 296 sorbates with little electron donating basicity and polarizability (i.e., $B \approx 0$ and $S \approx 0$) have

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297 Freundlich coefficients almost entirely dependent on dispersive forces (the V term). This
298 is, perhaps, unsurprising and is consistent with observations.

299 The Freundlich exponent, n , captures the non-linearity of the sorption process,
300 and, in the case of sorption from water to water-wet char, this exponent exhibited a
301 dependence on dispersive forces and polarity (i.e., the V and S terms, respectively). Note
302 that the slope of the line is not significantly different from 1 (1.19 ± 0.36), indicating that
303 Equation 7 is capturing the right dependencies of n on sorbate properties, but the low R^2
304 (0.47) suggests the correlation does not perform with much precision). The S parameter
305 has been correlated with the Freundlich exponent in studies of sorption of organic
306 chemicals to peat soil and GAC [32, 38]. For GAC (Darco 20-40 mesh from Sigma-
307 Aldrich), Shih and Gschwend [32] noted that the electron donating basicity (B term)
308 made a small contribution to the Freundlich exponent, but this was not observed for our
309 char perhaps due to differences in the oxygen functionality of the materials. For nonpolar
310 compounds (e.g., with $S \approx 0$), the dispersive forces dominate the sorption behavior. For a
311 typical polar sorbate (e.g., with $V \approx 1$ and $S \approx 0.5$), the Freundlich exponent will have
312 roughly equal contributions from the dispersion and polarity terms, but these will be
313 dominated by the constant (+1). We note that the constant in the n expression for our
314 char (+1) was greater than seen previously for GAC (+0.76) [32]; this could imply that
315 the isotherm nonlinearity also has some dependency on sorbent properties (e.g., GAC vs.
316 wood char). For example, the exponent could capture the chemical nature of the char
317 surface and physical distribution of pore spaces. The Freundlich exponents for char were
318 systematically higher than those for GAC [32] (Supplemental Data, Table S2) and, as
319 noted earlier, could not be predicted by the same LFER. Knappe's group has

320 demonstrated that pore structure and surface composition (e.g., oxygen content) have a
321 significant influence on the sorption behavior of organic chemicals [39,40], and
322 differences in the physicochemical profile of the sorption surface may explain apparent
323 differences in sorption properties of distinct BCs. Thus, sorbent-specific free energy
324 relationships may be needed for distinct types of black carbon sorbent materials.

325

326

CONCLUSIONS

327

328 Overall, three primary lines of evidence support the results presented here and
329 build confidence in this sorbent characterization approach: (1) the Freundlich parameters,
330 K_f and n , individually make sense (e.g., polar compounds have n values closer to 1 and
331 hydrophobic sorbates have larger K_f); (2) the ppLFFER yielded four best-fit parameters
332 (i.e., v_1 , v_2 , b_1 , and s_2 in Eqns. 3 and 4) that were significantly different from zero from
333 128 individual observations; and (3) previous researchers have also observed positive
334 relationships between K_d and V and negative relationships between K_d and B for similar
335 forms of black carbon. Further, the fit also indicates that considering sorption as a
336 function of the degree of surface saturation (where complete saturation is assumed to
337 correspond to saturation in solution) yields a ppLFFER that is understandable with respect
338 to sorbate-sorbent interactions.

339

340

341

342

Moreover, our results support the hypothesis that two distinct types of black
carbon, GAC and wood char, interact with organic sorbates *via* subtly different
combinations of intermolecular interactions, which arise from the physical and chemical
character of the respective sorbent materials. This implies a need for sorbent-specific

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343 black-carbon distribution coefficients in order to predict contaminant distribution in
344 natural sediments or amended cleanup sites. Fortunately, we found that a relatively small
345 set of sorbate probe compounds can be used to generate a ppLFER that enables
346 estimation of BC-water distribution coefficients for sorbates of interest where sorption
347 data are unavailable (with the caution that the ppLFER should be used within the
348 investigated Abraham/McGowan parameter space (Table 1)). Further work needs to be
349 done to extend the tested parameter space, being sure to utilize sufficient incubation times
350 to insure solution-sorbent equilibration.

351 Furthermore, natural systems with more than one source of BC may require
352 quantification of each BC type to accurately predict contaminant distribution. While
353 independent measures to quantify distinct BC fractions are available, no single method
354 exists to differentiate all possible fractions of BC in environmental matrices. Such a
355 method would be useful if important chemical differences between BC types are
356 confirmed.

357

358 SUPPLEMENTAL DATA

359 Wood char characteristics, previously modeled black carbons and their sorbent
360 parameters, toluene equilibration timescale for water-wet char, and comparison of
361 Freundlich exponents between GAC and char.

362

363 ACKNOWLEDGMENT

364 The authors thank J. MacFarlane, M. Streng, Z. Henrot, and E. Forsley. This material is
365 based upon work supported by the U.S. Army Corps of Engineering, Humphreys

366 Engineer Center Support Activity under Contract No. W912HQ-10-C-0005 awarded as
367 part of the SERDP program. The authors do not have any conflicts of interest to disclose.

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510

FIGURE LEGENDS511 **Figure 1. Dominant sources of biochar and illustrated pore and surface structures.**

512 Biochar is a ubiquitous sorbate that has natural, incidental, and engineered sources. The
513 arrow thicknesses indicate the postulated relative sizes of the predominant source terms
514 [22-24]. Biochars are formed from the incomplete combustion of biological material,
515 such as wood, leaves, husks, and grasses, and often have microstructures that reflect the
516 structure of the original biological material. (Wood char is depicted here). On the
517 molecular scale, biochar is characterized by a highly aromatic surface with some oxygen
518 content and can interact with sorbents, such as nitrobenzene, via electron donor-
519 acceptor and van der Waals interactions.

520

521 **Figure 2. Freundlich isotherms for 14 probe sorbates on chestnut wood char. Solid**

522 and dashed lines are best-fit curves, from which we derive characteristic Freundlich
523 parameters, $\log K_f$ (intercept) and n (slope). See Table 2 for parameter values.

524

525 **Figure 3. Overall correlation of the individual observed sorption coefficients with**

526 **the predicted sorption coefficients.** Predicted values were determined using the
527 ppLFER given by Equation 4, whereas the observations were experimentally determined
528 from the 128 individual equilibrium experiments conducted in the present study.

529

530 **Figure 4. Correlations of observed Freundlich coefficients, K_f [(mg/kg)/(mg/L)ⁿ], and**
531 **the Freundlich exponent, n , with ppLFER-predicted values for those parameters.**

532 Predicted values were determined using Equations 6 and 7. Diagonal dashed lines are the

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533 one-to-one lines, while solid lines are linear best fits. Error bars represent one standard
534 deviation; invisible error bars are smaller than the symbol.